

## ATTACHMENT C

### Amendments to the Claims

*This listing of claims will replace all prior versions, and listings, of claims in the application.*

1. (Currently Amended) A method for industrial production of high dispersed powders, comprising the steps of:

mixing where material to be pulverized is mixed with high pressure working gas into a gas-solids suspension,

conveying of the gas-solids suspension which is through acceleration nozzles conveyed to the a pulverizing chamber of a counterjet pulverizer for autogenic pulverizing, characterized in that

conveying the pulverized gas-solids suspension is conveyed at least to one an intermediate tank, said steps of mixing, conveying to a pulverizing chamber and conveying to an intermediate tank comprising a in the pulverizing cyclecircle,

removing where the gas is removed from the gas-solids suspension and blend and collecting the solids collected into the intermediate tank,

returning solids from the intermediate tank which are returned to be pulverized together with new raw material till there is in the equipment a desired wanted circulation load, and

continuing whereafter the process continues so that as much end product material is removed from the process it as ready product raw material is added to it the process, and

wherein said mixing step includes the step of

feeding the material alternately into side by side double-valve feeders and balancing tanks, where a feed pressure in each double-valve feeder is higher than a regular feed pressure in an associated balancing tank, and

synchronizing the double-valve feeders so that an after-pressure left in one double valve feeder after release of the material into the associated balancing tank is

utilized as initial pressure in the other double-valve feeder after receipt of material therein.

2. (Currently Amended) A method according to claim 1 characterized in that the\_a pulp density of the solids collected into the intermediate tank is raised by means of a pressing screw conveyor before returning the solids to the counterjet pulverizer.

3. (Currently Amended) A method according to claim 1, wherein characterized in that material to be pulverized is fed to counterjet pulverizer through double valve feeder and balancing tank, whereby in double valve feeder a feed pressure higher than the regular feed pressure is used and the conveying of the gas-solids suspension flow of counterjet pulverizer working gas is broken or choked for a while, when the lower valve of each double-valve feeder is opened.

4. (Currently Amended) A method according to claim 3, wherein characterized in that pulverizing is carried out at least in two counterjet pulverizers, whereby there is in one of them said counterjet pulverizers conventional acceleration nozzles and in the other of said counterjet pulverizers acceleration nozzles furnished with gas outlet channels for effective pulverizing of high dispersed material.

5. (Canceled)

6. (Currently Amended) A method according to any above claim 1, further including the steps of: characterized in that removing the end product removed from the intermediate tank, conveying the end product is conveyed to a separate mechanical classifier outside the pulverizing circulation circle cycle, separating of where the greatest sized particles are separated from the end product, and returned returning the greatest sized particle to the intermediate tank for an additional pulverizing circulation cycle.

7. (Currently Amended) A method according to claim 1, further including the step of programming, characterized in that in order to ensure the a uniformity of the end product quality, there is in the equipment a control unit with, into which the limit values of the selected most important parameters of the pulverizing process, the parameters being selected from the group comprising as the a) a quantity of raw material, b) a volume, a pressure and a temperature, of a working gas, c) a quantity of energy used for working gas pressurization, and d) a quantity of the circulation load are programmed.

8. (Currently Amended) A method according to claim 1, wherein characterized in that the pulverizing conditions are regulated so that there is in the end product a portion of particles aimed at in a granular class of 0.2-5 0,2-5 $\mu$ m.

9. (Currently Amended) A method according to claim 8, wherein characterized in that in the project the material to be pulverized is circulated between 2 – 10 times, advantageously 4-7, in order to achieve the a set granular class.

10. (Currently Amended) A method according to claim 6, wherein characterized in that the coarse product greatest sized particles separated by classifier is are returned to intermediate tank using as a pneumatic transfer from the intermediate tank of the double-valve feeder after initial pressurizing by means of the initial pressure release gas.

11. (Currently Amended) A method according to claim 1, further including the step of characterized in that pre-pulverizing the raw material pre-pulverized by with a mechanical pulverizer is used as raw material.

12. (new) A method according to claim 9, wherein the material to be pulverized is circulated between 4 – 7 times.